



# Review of Rubber Mixing & Effect on Polymer / Compound Performance

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Review of Mixing

Introduction Mixing of SBR Mixing of NR/BR/SBR Mixing of EPDM CB Dispersion in SBR Conclusion





Introduction Mixing of SBR Mixing of NR/BR/SBR Mixing of EPDM CB Dispersion in SBR Conclusion



# Mixing gives reason to changes of ingredients and of reactions between the ingredients

- $\lambda$  Mixer behaves like a reactor
- $\lambda$  In addition to mechanical work on distribution and dispersion

## Polymer Changes

- $\lambda~$  MW, MWD and LCB
- $\lambda$  Radical reactions of polymer with Carbon Black
- Protection / Processing Aids
  - $\lambda$  Ingredients with functional groups reacting with polymer
  - $\lambda$  Acid / Base Reactions

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## Mixing <u>What is the goal of Mixing?</u>

- λ Compound, which can be processed in the desired machines, turned into a part, which meets customer expectations
  - Viscosity of compound processing
  - <u>Dispersion of Filler physical</u> properties
  - v Homogeneity
  - v Rheology Cure kinetic





Jan. 21, 1958

AGENT

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## Mixing <u>What is the conflict in Mixing?</u>

- $\lambda$  Viscosity of compound:
  - Viscosity correlates to MW: Performance – Higher is better Processing –
    - λ Lower is better: IM
    - <sup>λ</sup> Higher is better: CM, Extrusion
- $\lambda$  Dispersion of Fillers
  - Temperature rise through high shear correlates to:
    - MW (+ Type of Polymer),
      Filler (Type) / Oil loading
- $\lambda$  Rheology Cure kinetic





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Source: Thesis Ebell

# Process factors in order of importance

- $\lambda$  Mixing Time or Mixing Unit Work
- $\lambda$  Rotor Speed
- $\lambda$  Mixer Temperature
- $\lambda$  Ram Pressure
- $\lambda$  Fill Factor (not independent from Ram Pressure)

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Source: Sommer, R Handbook

# Mixing / molecular weight change

- λ MW of different NR-Types coagulated and stabilized
  - Bimodal MW distribution
  - v MWD of 5 10
- $\lambda$  Mastication on Mill of SMR 20
  - v MW decreases
  - Bimodal MW distribution becomes a broad MW



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	Conclusion	Source: Thesis Ebell

Mixing of SBR:

## Mooney Viscosity over Mixing Time \*)



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Source: Martin, RCT 1955 Fig left: Thesis Ebell

## Mixing of SBR:

Dependence of physical properties on Mooney viscosity of masticated SBR rubber and on temperature of mastication.

#### Correlation of Mooney Viscosity with Tensile Strength (obtained from 5 Factor Mixing Design)



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Source: Ebel, Thesis

# Mixing of SBR:

#### Mooney Viscosity over Unit Work & Rotor Speed (no correction of Ram Pressure & Mixer Temperature & Fill Factor)



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Source: Ebel, Thesis

# Mixing of SBR:

#### **Tensile Strength over Unit Work & Rotor Speed**

(no correction of Ram Pressure & Mixer Temperature & Fill Factor)



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Source: Ebel, Thesis

## Mixing of SBR:

- $\lambda~$  Mix Time over Unit Work & Rotor Speed
- $\lambda$  Ram pressure 0.22 (left)

- 0.80 (right)



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Source: Ebel, Thesis

## Mixing of SBR:

### λ Dump Temperature over Unit Work & Rotor Speed

 $\lambda$  Ram pressure 0.22 (left)

- 0.80 (right)



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Source: Ebel, Thesis

## Mixing of SBR:

- $\lambda$  Tensile over Unit Work & Rotor Speed
- $\lambda$  Ram pressure 0.22 (left)

- 0.80 (right)



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Source: Ebel, Thesis

## Mixing of SBR:

- $\lambda$  Tensile: Predicted versus Actual (left)
- $\lambda$  Mooney Viscosity: Predicted versus Actual (right)



Mixing of SBR Mixing of NR/BR/SBR Review of Mixing Mixing of EPDM **CB** Dispersion in SBR Conclusion Source: Ebel, Thesis Factors Tool Design-Expert® Software Overlay Rdt Factor Coding: Actual 75.00 Original Scale (median estimates) Gauges 🚆 Sheet 📒 Dump Temp 160000 **Overlay Plot** Tensile: 10300 Mix Time DumpTemp 156000 Default Dump Temp 69.00 Mooney Visc Tensile 9500 Speec Tensile X1 A:Unit Work Design Points 63.00 X1 = A: Unit Work Mone/\isc 67.000 X2 B:Rotor Speed Rotor X2 = B: Rotor Speed NikTine 210000 NikTine 230000 Money\isc 65000 Actual Factors C:Fill Factor C: Fill Factor = 0.80 'n 57.00 D: Ram Pressure = 0.40 E: Temp Mixer = 50.00 D:Ram Pressure + 51.00 50.00 4500 Term 675.00 900.00 975.00 1050.00 1125.00 1200.00 600,00 75000 825M

A:UhitWork

## Mixing of SBR: Unit Work over Rotor Speed

 $\lambda$  Tensile at 10.3 MPa (max. value)

Introduction

- $\lambda$  Mixing time 210 230 sec
- $\lambda$  Mooney viscosity ML(1+4) 100°C: 65 67 Mooney Units

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Source: Kreuzwieser, Thesis



## Mixing of NR/SBR/BR:

- $\lambda$  MI(1+4)100°C over Mixing Time & Rotor Speed
- $\lambda$  Mastication time 30 sec (left)

70 sec (right)

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Source: Kreuzwieser, Thesis



## Mixing of NR/SBR/BR:

- $\lambda$  Specific Energy Mix over Mixing Time & Rotor Speed (left)
- $\lambda$  Correlation of Mooney with Specific Energy Mix (right)



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Source: Kreuzwieser, Thesis



### Mixing of NR/SBR/BR:

 $\lambda$  Extrusion over Mixing Time & Rotor Speed

(Extrusion Experiment at constant Screw speed 50 rpm)

- Extrusion Motor power consumption (Nm) (left)
- v Extrusion Head Pressure (bar) (right)
- $\lambda$  Extruder Output at 50 rpm is invariant towards head-pressure.



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Source: Kreuzwieser, Thesis

### Mixing of NR/SBR/BR:

- $\lambda$  Tensile Strength over Mixing Time & Rotor Speed
  - v Mastication time has little to none influence



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Source: Kreuzwieser, Thesis



#### Mixing of NR/SBR/BR:

- λ CB Distribution over Mixing Time & Rotor Speed
  - v 30 sec Mastikation time (left)
  - v 50 sec Mastikation time (right)
    - **λ 70 sec Mastikation time (lower right)**



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#### Review of Mixing

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B: mixing

Introduction Mixing of SBR **Mixing of NR/BR/SBR** Mixing of EPDM CB Dispersion in SBR Conclusion



Source: Kreuzwieser Thesis

## Mixing Time – VAW concentration

## $\lambda\,$ Tire Tread Compound



**B: Mix Time** 

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Source: Nijmann Vredestein

## **Effect of Polymer Structure on Mixing**

- $\lambda$  Influence of branching
- $\lambda\,$  Power consumption of the mixer and batch temperature in the mixing phase due to EPDM LCB (Mixer: W&P, GK90E, Rotor



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## Viscosity Drop during mixing

- λ Mastication of EPDM
  Change of MW Distribution
  curve depends on MW and
  MWD
  - Most rubbers show decrease in viscosity, if exposed to mechanical and heat energy.
  - Molecular weight curve will change it size and form!

**GPC Eluation Time** 

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Source: S.Yu, H-J Graf



- Due to mixing there is a shift of λ **GPC** average MW (Note the GPC-MW / Mooney **Correlation**)
- λ Polymers of different origin behave different
- High MW Polymers effected more λ than low MW Polymers









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Source: HJ Graf

### Mixing experiment with EPDM low (*left*) MW / high MW (*right*) Tensile strength [MPa]



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Source: HJ Graf

### Mixing experiment with EPDM low (*left*) MW / high MW (*right*) Crack Growth 25 (*top*) / 35 (*bottom*) (mm/cycle 10^-5)



Function / Use of Process Aids <b>Mixing of Compound</b> Meeting a Specification Compound to Cost Methods in Development	Introduction <b>Effects of mixing on Polymer</b> Incorporation of Fillers Mixing of Oil Interaction of Ingredients	HJG
Compound DoE&Simulation Reverse Development Compound Exercises	Acceleration in the mixer / mill Mixing Recipe Design in consideration of formula Summary	Source: HJ Graf

# Mixing experiment with EPDM low (*left*) MW / high MW (*right*) Fatigue to falilure (cycles)



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Source: Cotten, RCT 58

## Influence of CB Properties Polymer CB-441 at loading of CB 50 phr

#### Incorporation Time over CTAB and DBPA of Carbon Blacks

Acc.: Cotten RCT 58 (1985)



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Source: Cotten, RCT 58

## Influence of CB Properties Polymer CB-441 at loading of CB 50 phr

#### Bound Rubber over CTAB and DBPA of Carbon Blacks

Acc: Cootton, RCT 58 (1985)





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Source: Hess, RCT 57

## Properties of Carbon Black influence the mixing process and the properties of the compound

- $\lambda$  DOE with Carbon blacks
  - DOE map according to available CB grades
  - CB-Dispersion on SBR 1500 compound as a function of CB surface area and DBPA at to different mixing procedures
    - λ CB and oil added separately
    - $^{\lambda}$   $\,$  CB added with black  $\,$
    - SBR 1500 with
      60 phr CB
      37,5 phr oil

According to modern DoE Programs: lack of statistic significance.



DBPA, cm3/100g

110

120

ADDED WITH B

B 120

AREA,

SURFACE

NITROGEN

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Source: Hess, RCT 57

## **Addition of Oil**

- λ In some rubbers oil must be added separately to achieve proper dispersion of CB
  - SBR 1500 needs separate addition of oil.
  - Otherwise compound will not take up enough shear for dispersion

According to modern DoE programs lack of statistic significance



SBR 1500 Compound with 10 phr, 25 phr and 40 phr Oil

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Source: Hess, RCT 57

#### SBR 1712 – Mixing dependent on CB DBPA-Absorption & N<sup>2</sup> Surface

λ But the Statistic models are not significant



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Source: Hess, RCT 57

#### SBR 1712 – Mixing dependent on CB DBPA-Absorption & N<sup>2</sup> Surface ???

- λ But the Statistic models are not significant
  - <u>Mix Energy to 95% Dispersion Predicted vs Actual (left)</u>
  - **<u>W</u>** But Correlation of Dispersion Index with Factors are significant (right)





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Source: Exxon

## Filler / Oil ratio of Rubber due to processing window in mixing

 $\lambda\,$  Viscosity (or MW) dependent ability to load with carbon black and

oil



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Source of Slide: Exxon

## **Conclusion / Important to remember:**

- $\lambda\,$  SBR requires high rotor speed and longer mixing time resp. Energy input
- λ NR (Blend) requires medium to high rotor speed and sufficient time for maximum performance.
   Temperature should be kept under control
- $\lambda\,$  EPDM requires lower rotor speed and mixing time as short as possible
- λ Carbon Black Dispersion experiment should be re developed (statistic significance not sufficient) We should redo this experiments!